

Carbon dioxide-expanded liquid substrate phase: an effective medium for selective hydrogenation of cinnamaldehyde to cinnamyl alcohol

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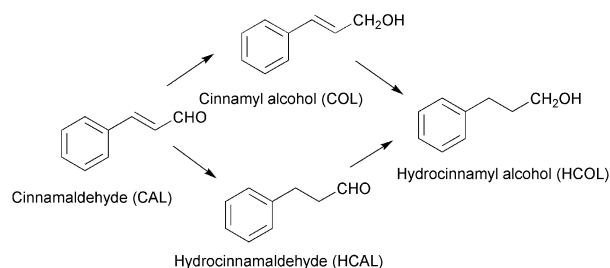
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It has been shown that CO₂-expanded cinnamaldehyde liquid phase is a unique and effective medium for cinnamaldehyde hydrogenation to cinnamyl alcohol, due to interactions between the C=O group of the substrate and CO₂ molecules and increased solubility of H₂.

The use of supercritical carbon dioxide (scCO₂) as an environmentally benign solvent for organic synthetic reactions is currently receiving much attention. However, a drawback of scCO₂ prevents its utilization in homogeneous catalytic synthesis, due to its low ability to dissolve organometallic complexes. Some attention has been paid to enhancing the solubility of metal complexes in scCO₂ by using ligands with an affinity for CO₂.^{1,2} Is the homogeneous phase really efficient for all the catalytic reactions in scCO₂? It was reported that insoluble rhodium complexes exhibited high activity and selectivity for hydroformylation of 1-hexene in scCO₂,³ and a faster reaction rate was obtained in two-phase than in single-phase for α -pinene hydrogenation in scCO₂ with Pd/C catalysts.⁴ Moreover, scCO₂ was reported to be dissolved in organic liquid substances and, in some cases, the solubility of CO₂ can approach a value much higher than 80 mol% in the vicinity of mixture critical point. The dissolution of CO₂ in an organic solvent is also accompanied by a significant volumetric expansion of the liquid phase. Subramaniam and Busch reported that CO₂-expanded CH₃CN solvent is an effective reaction medium for cyclohexene oxidation with TPP/FeCl catalyst.^{5,6} And an increase in enantioselectivity has recently been reported for asymmetric hydrogenation of atropic acid in CO₂-expanded [bmim]PF₆ phase.⁷ In the present communication, we will show that CO₂-expanded cinnamaldehyde (CAL) liquid phase using no organic solvent is a significantly effective medium for its selective hydrogenation to cinnamyl alcohol (COL) (Scheme 1) and that this is due to interactions between the substrate and CO₂ molecules, confirmed by *in situ* FTIR, and increased H₂ concentration in the liquid phase.

Table 1 shows the results of CAL hydrogenation and phase behaviour observations.[†] When the quantity of CAL was 0.2 mmol

and that of Ru complex 0.075 or 0.15 μ mol, the reaction system was in a single phase and the selectivity of COL was smaller than 30% (entries 1, 2). When 0.68 μ mol of Ru complex was used at a higher CO₂ pressure of 16 MPa, the total CAL conversion increased to 55% while the COL selectivity did not change (entry 3). Under the conditions for this run, the system was in a two-phase mixture including a small volume of CAL-rich liquid phase. In addition, CAL hydrogenation was also examined under solvent-less conditions and in high pressure N₂ and CO₂ under two-phase conditions with using a large amount of CAL of 7.5 mmol (entries 4–7). Under the solvent-less conditions, a high COL selectivity of 88% was obtained (entry 4). When the CAL liquid phase was pressurized by 8.5 MPa N₂ (entry 5), the total conversion and COL selectivity did not change compared to these obtained under solvent-less conditions. However, 8.5 MPa CO₂ was used instead of N₂, the total conversion was enhanced to 24% from 11% and the COL selectivity to 91% from 88% (entry 6). When CO₂ pressure was further raised, the total conversion was further enhanced and the COL selectivity was also improved, which was 98% at 16 MPa (entry 7) in which the reaction mixture included a CO₂-rich gas phase and a large volume of CAL liquid phase dissolving CO₂ (CO₂-expanded liquid phase). Thus, the influence of phase



Scheme 1 Hydrogenation of cinnamaldehyde in compressed CO₂.

Table 1 Results of CAL hydrogenation with Ru complex in compressed CO₂

Entry	Ru/ μ mol	CAL/mmol	CO ₂ pressure/MPa	Conversion (%)	Selectivity (%)			Phase present ^a
					COL	HCAL	HCOL	
1	0.075	0.2	10	21	25	48	27	G
2	0.15	0.2	10	22	23	51	26	G
3	0.68	0.2	16	55	24	50	26	G ^b , L
4	50	7.5	—	11	88	9	3	G ^c , L
5	50	7.5	8.5 N ₂	12	88	10	2	G ^d , L
6	50	7.5	8.5	24	91	7	2	G, L
7	50	7.5	16	54	98	1	1	G, L

^a G: CO₂-rich gas phase, L: CO₂ expanded CAL liquid phase. ^b Very small droplets of CAL and/or catalyst were observed. ^c H₂-rich gas phase.

^d N₂-rich gas phase. Reaction conditions: bis(pentafluorophenyl)phenylphosphine/Ru = 3; H₂ pressure, 4 MPa; temperature, 50 °C; reaction time, 2 h. The Ru complex is completely soluble in CAL under these conditions used.

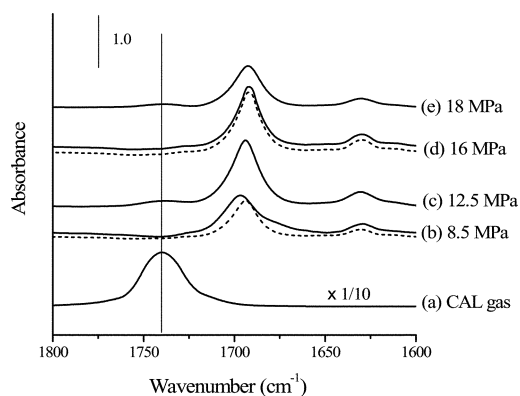


Fig. 1 FTIR spectra of pure CAL (gas) and CAL dissolved in compressed CO₂ as well as in H₂ and CO₂ mixture (dotted line) at 50 °C.

behaviour was significant and the presence of high-pressure CO₂ was requisite for selective CAL hydrogenation.

The present results demonstrate that larger conversion and larger COL selectivity can be obtained for CAL hydrogenation in CO₂-expanded CAL liquid phase. A few factors should be taken into account to explain these results. (1) CAL concentration. Although CO₂ and H₂ are dissolved in the CAL phase, the CAL concentration is still large in this phase. High CAL concentration was previously reported to benefit the formation of COL with heterogeneous catalysts.^{9,10} (2) H₂ concentration. The concentration of H₂ in the CO₂-expanded CAL phase should be larger compared with that in the absence of CO₂ because a large quantity of CO₂ dissolved in the CAL phase favors the dissolution of H₂. (3) Compressed CO₂. The mass transfer resistance and substrate inhibition, if existed, should be reduced in CO₂-expanded CAL and scCO₂ phases. Note that compressed CO₂ increases the CAL conversion and the COL selectivity but compressed N₂ does not; hence, hydrostatic pressure to the CAL liquid phase is insignificant. So, direct effects of CO₂ may be assumed, and this was examined by FTIR. ‡ Fig. 1 shows FTIR spectra from 1800 to 1600 cm⁻¹ for CAL molecules dissolved in different gaseous mixtures at 50 °C. The spectrum (a) is a reference of gaseous pure CAL, indicating $\nu(\text{C}=\text{O})$ at 1740 cm⁻¹. $\nu(\text{C}=\text{C})$ was too weak under the conditions used. The absorbance in N₂ was very weak due to a less solubility of CAL in N₂. In contrast, CAL can be more soluble in dense CO₂, leading to stronger absorption (b–e). The absorption of $\nu(\text{C}=\text{O})$ in dense CO₂ red-shifted compared with gaseous CAL and $\nu(\text{C}=\text{C})$ appeared at 1630 cm⁻¹ in 8.5 MPa CO₂. Further it was red-shifted a little with increasing CO₂ pressure. The dotted lines show the results in the presence of 4.0 MPa H₂, which has only a marginal effect. Moreover, the absorbance of $\nu(\text{C}=\text{O})$ of CO₂ split into two peaks at 8.5 MPa from a single peak at 1.5 MPa, and these peaks split further to four peaks in the presence of CAL (Fig. 2), indicating the existence of interactions between CAL and CO₂ molecules in a gas state. For a CO₂ molecule, the carbon atom is partially positive and the oxygen atoms are partially negative. Thus, a C–H...O hydrogen bond should exist between CO₂ molecules and carbonyl groups even though it is weaker than O–H...O bonds.¹¹ The specific interaction of CO₂ molecules with Lewis base groups, especially carbonyl groups, through a C–H...O hydrogen bond has been reported.^{11,12} In addition, interactions are known to exist between CO₂ and transition metal complexes, as reviewed by Leitner.¹³ We may assume that the above mentioned interactions exist in the CO₂-expanded CAL liquid phase as well.

When the reaction occurs in the CO₂-expanded CAL phase, the high H₂ concentration (factor 1) is chiefly responsible for the increased CAL conversion and the high CAL concentration (factor

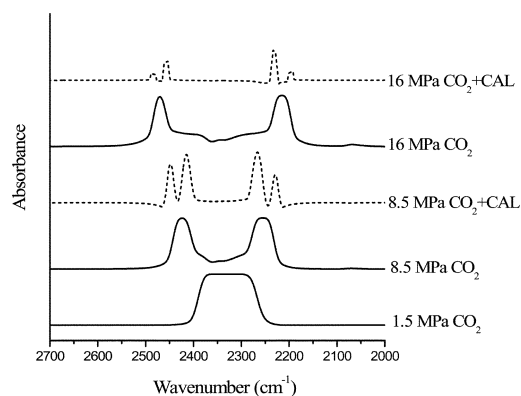


Fig. 2 FTIR spectra of pure CO₂ and mixture of CO₂ and CAL at 50 °C.

2) and CAL–CO₂ interactions (factor 3) for the high COL selectivity. The interactions may make the carbonyl group of CAL molecules more polar and reactive. It still remains unsolved whether CO₂ molecules have effects on the specific activity of the Ru complex in the CO₂-expanded CAL liquid phase (and in the CO₂-rich gas phase). For a catalyst of supported metal particles, direct effects of CO₂ on their properties were previously suggested.¹⁴

In summary, the CO₂-expanded substrate liquid phase has potential as a green reaction medium that does not need additional organic solvent.

Notes and references

† Hydrogenation of CAL in scCO₂ was carried out at 50 °C in a 50 mL high-pressure stainless steel reactor and a catalyst prepared from RuCl₃ and bis(pentafluorophenyl) phenylphosphine was used. This ligand was selected due to its high effectiveness in scCO₂ and the method of Ru complex preparation was described elsewhere.⁸ The phase behavior and solubility of Ru complex and CAL in pure CO₂ and in H₂ + CO₂ were examined by visual observations with a 10 mL high-pressure sapphire-windowed view cell.⁸ The reaction was conducted under different conditions, at which the reaction system was homogeneous or heterogeneous.

‡ The FTIR spectra were measured with 0.01 mL CAL using a 1.5 mL high pressure cell in a path length of 4 mm at 50 °C.

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